

DEMOSOFC: first industrial size biogas-fed SOFC plant in Europe

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## H2020 Fuel Cells and Hydrogen 2 Joint Undertaking under Grant Agreement No. 671470 Demonstration of large SOFC systems fed with biogas from WWTP





ENERGY

**SOFC:** 

Highest efficiency in energy recovery from biogas 50-56%

Industrial size SOFC plant in Europe (110 kW<sub>e</sub> + 55 kW<sub>th</sub>) fed by biogas from sewage sludge







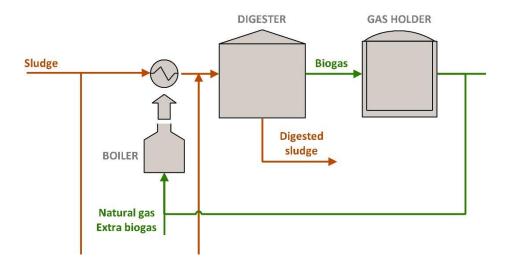


Imperial College



#### Plant layout







 Construction of a concrete basement with underground piping to host the cleaning system and the SOFC modules

Underground biogas pipes duct are separated from others for safety reasons

DEMOSOFC site before the project start



Concrete basement



→ Construction of a 100+ meters biogas pipeline to transfer biogas from the gas holder area to the DEMOSOFC area, and exchange water for heat recovery, compressed air and electrical connections.

Piperack





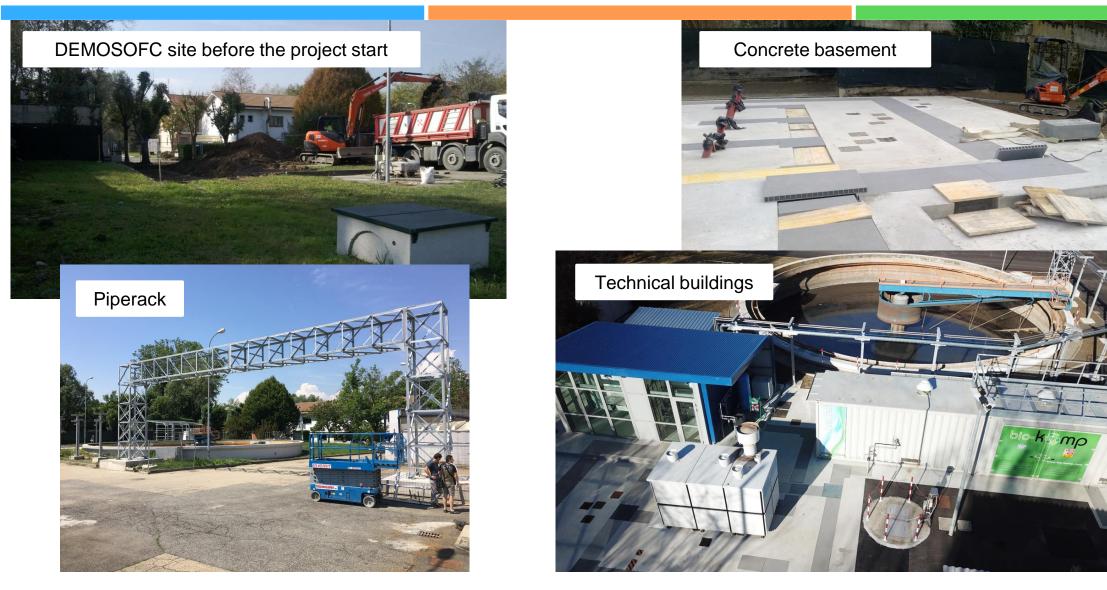
- → Construction of a dedicated building with 3 dedicated rooms for:
  - Electrical cabinets
  - Heat recovery pumps and collectors
  - Control room

#### Construction of other side-buildings for auxiliary gases and UPS.

Technical buildings

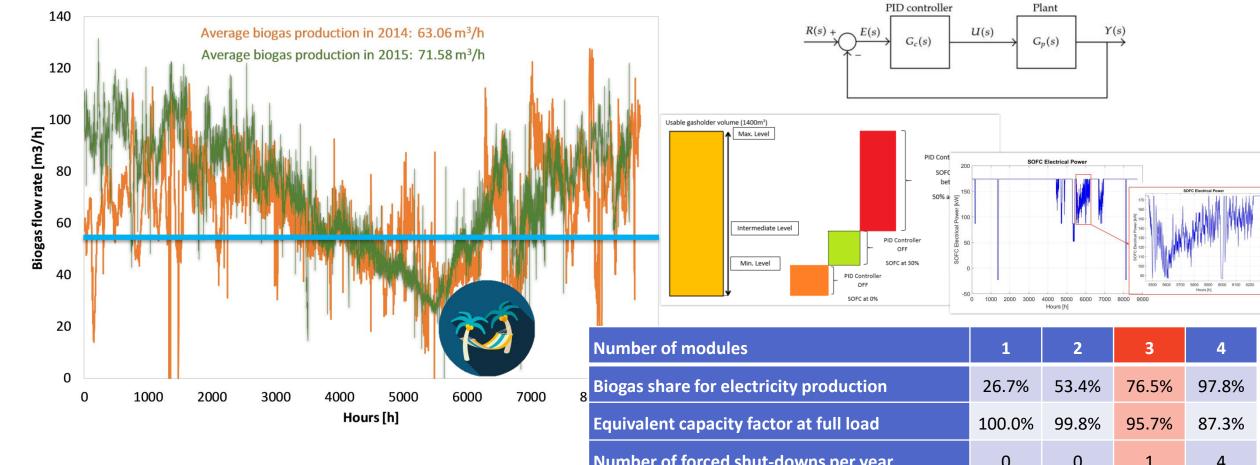






#### **Biogas production historical trend**



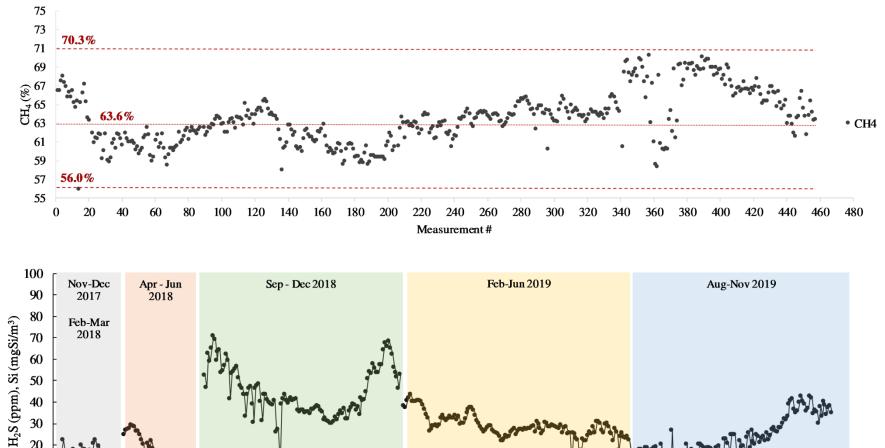


Biogas share for electricity production	26.7%	53.4%	/6.5%	97.8%	
Equivalent capacity factor at full load	100.0%	99.8%	95.7%	87.3%	
Number of forced shut-downs per year	0	0	1	4	
Average electrical efficiency	53.16%	53.15%	53.05%	52.66%	
Average thermal efficiency	80.00%	79.96%	79.09%	77.35%	

#### **Issue: Biogas purification**

180 200





220 240

Measurement#

		H <sub>2</sub> S (ppm)	Si (mgSi/m <sup>3</sup> )	CH <sub>4</sub> (%)
A	verage	28.66	3.78	63.57
	Min	0.00	0.00	56.04
	Max	71.05	9.43	70.35



Contaminants

## Selection of the sorbents



#### 1. Sorbents selection

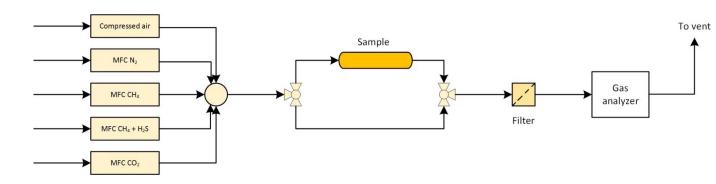
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From:	Producer & Product	Suggested for:	Datasheet performance	Cost	Unit
	SulfaTrap R8G	Siloxanes, large size sulphur compounds and low H <sub>2</sub> S levels removal	30-70 mgS/g on biogas @ 2000 ppm(v) H <sub>2</sub> S	15.88	€/kg
	AirDep CKC	$H_2S$ removal	> 200 mgS/g on air	2.80	€/kg
	AirDep CKI	H <sub>2</sub> S removal	> 200 mgS/g on air	5.00	€/kg
	AirDep C64	Siloxanes removal	600 mgCCl <sub>4</sub> /g on air	2.20	€/kg

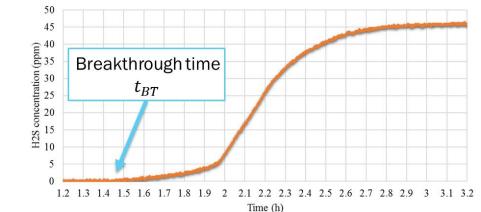




2. Lab activity

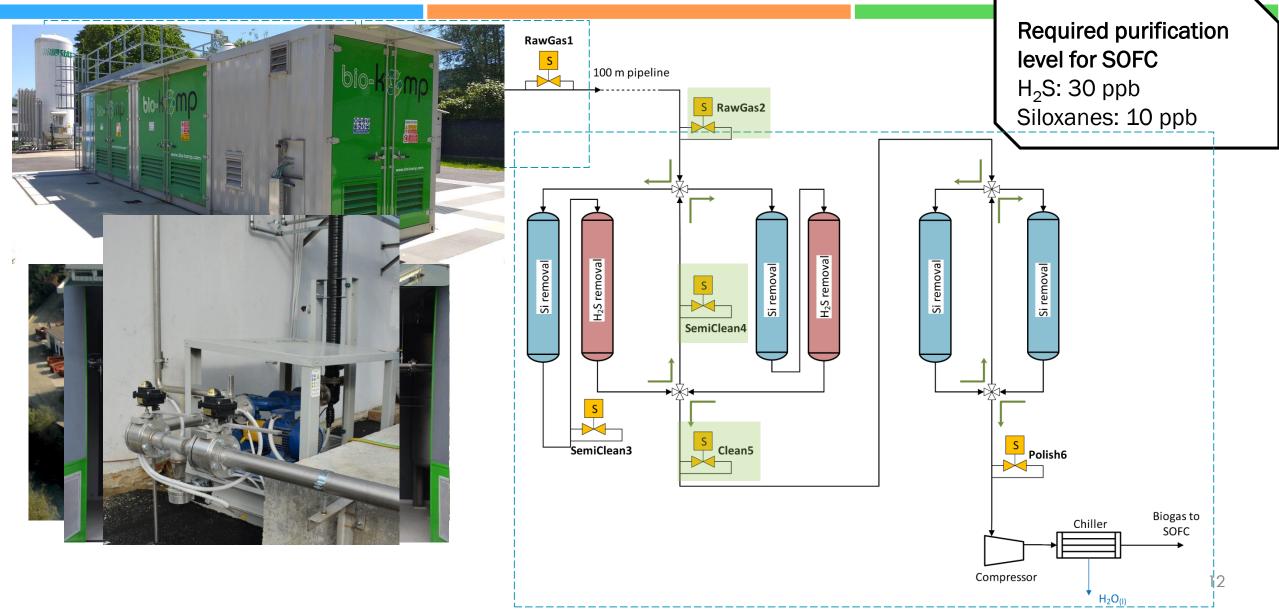


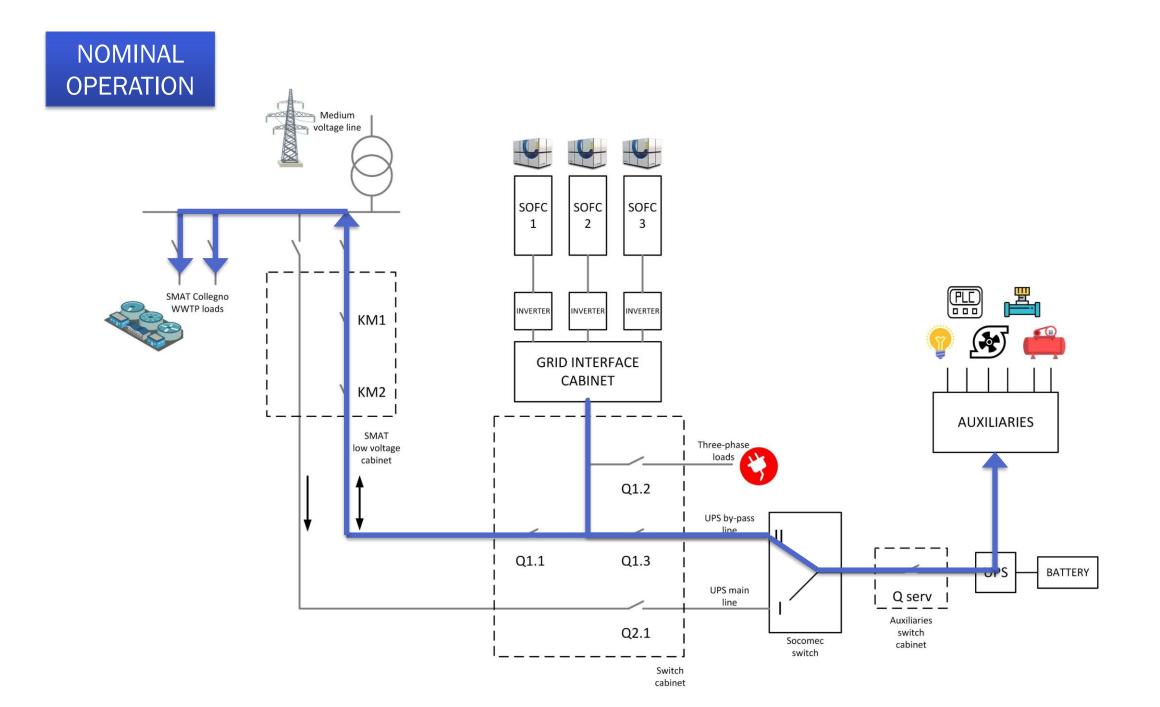
#### 3. Adsorption capacity



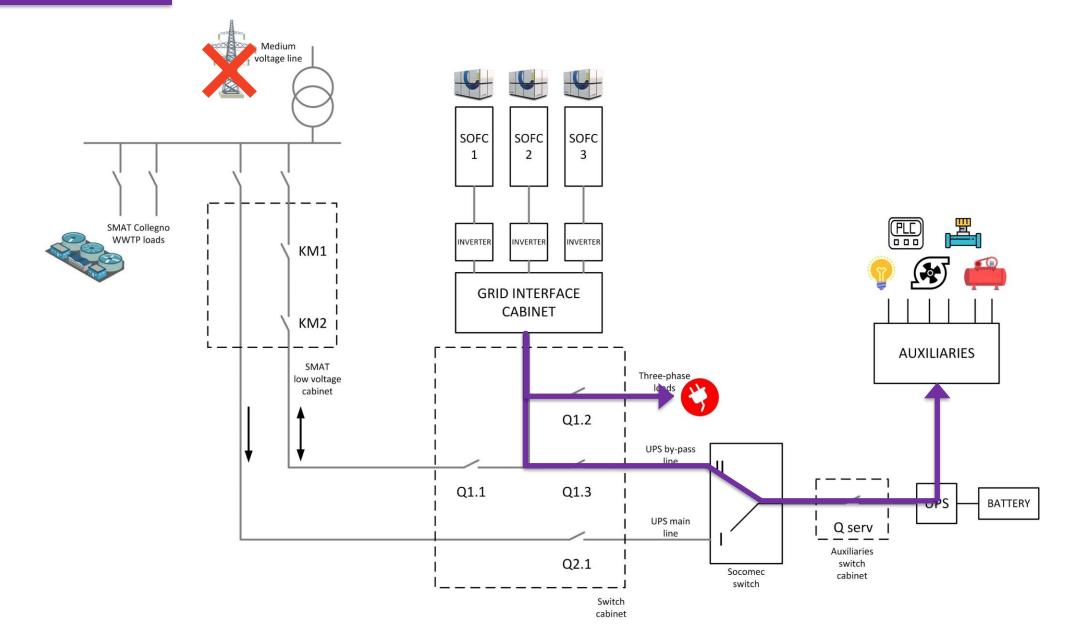
# Biogas purification system: lead & lag configuration (DEMOSOFC)





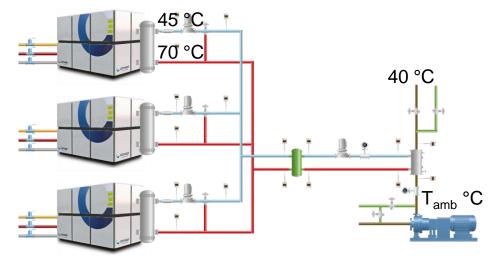


#### ISLAND MODE



#### Thermal recovery system and activities

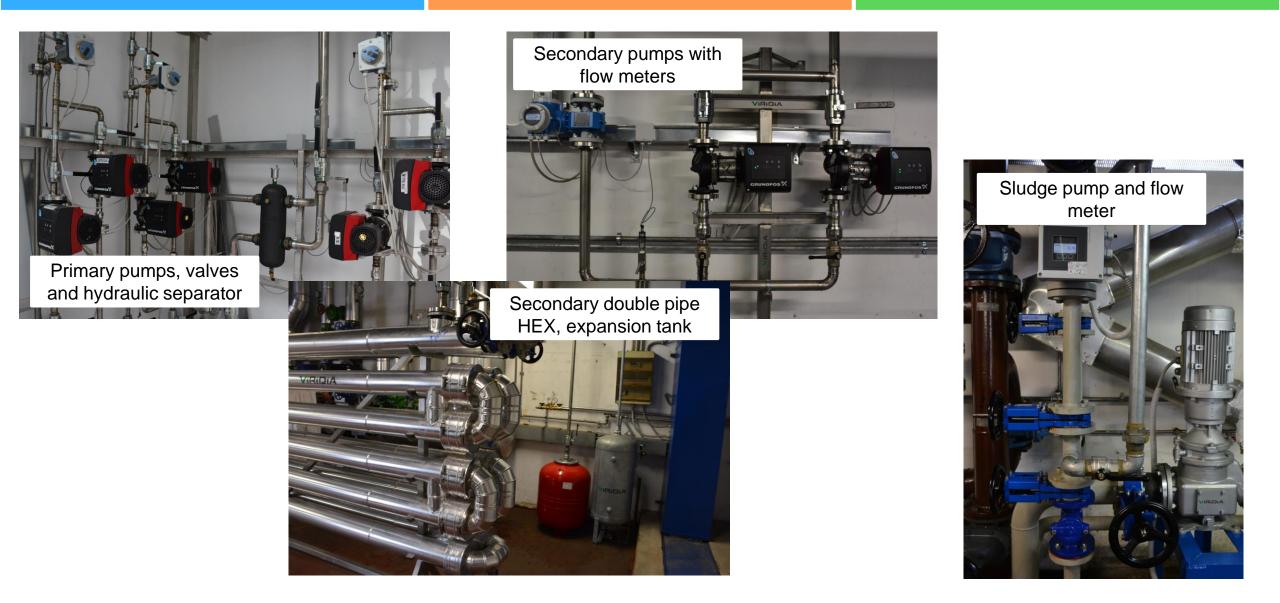
- Exhaust gases are found at around 200-250°C and are cooled down by controlling the water side (dew point is ~ 36 °C at full power but condensation should be avoided)
- → Thermal recovery on SOFC side is performed by using a mixture of water-glycol (30% glycol) with set-point temperatures of 45°C (inlet) and 70°C (outlet). Water flow rate is adjusted by using a dedicated PID controller.
- → A mixing valve, controlled by another PID, is used to guarantee 45°C at the HEX inlet and avoid condensation.
- → On the sludge side, sludge is heated up from ~ ambient temperature to 40°C (a PID controller is available to regulate the flow rate in order to guarantee a fixed outlet temperature)





#### Thermal recovery system and activities



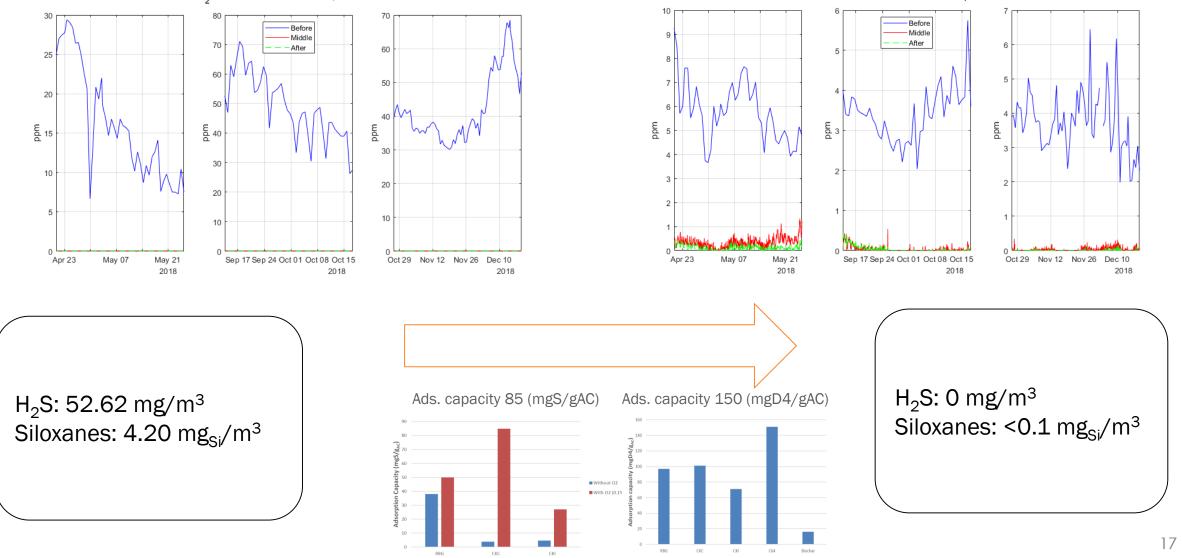


#### **Biogas clean-up**



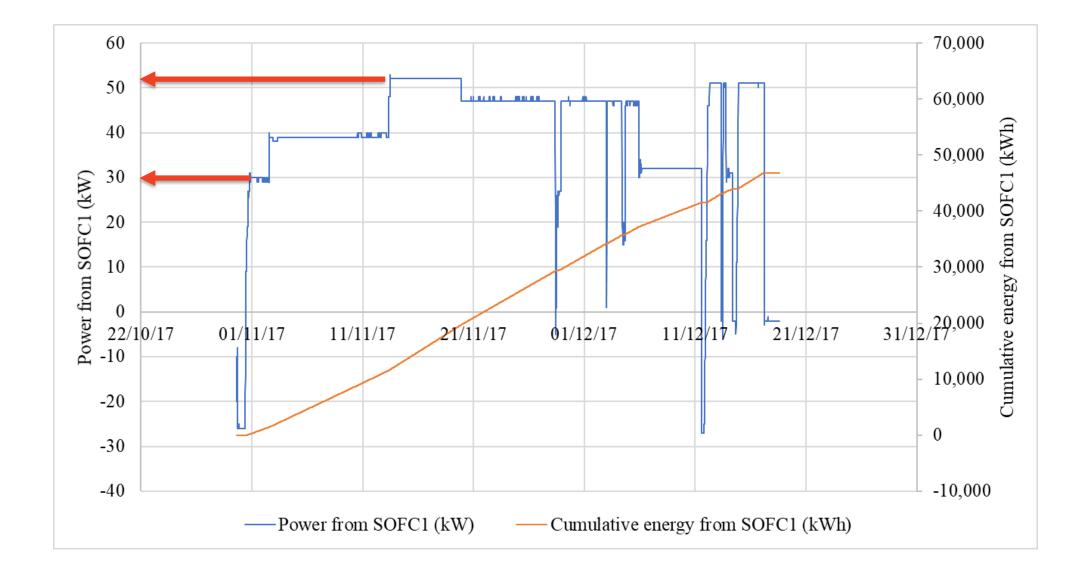
Siloxanes concentration - Clean-up unit

H<sub>2</sub>S concentration - Clean-up unit



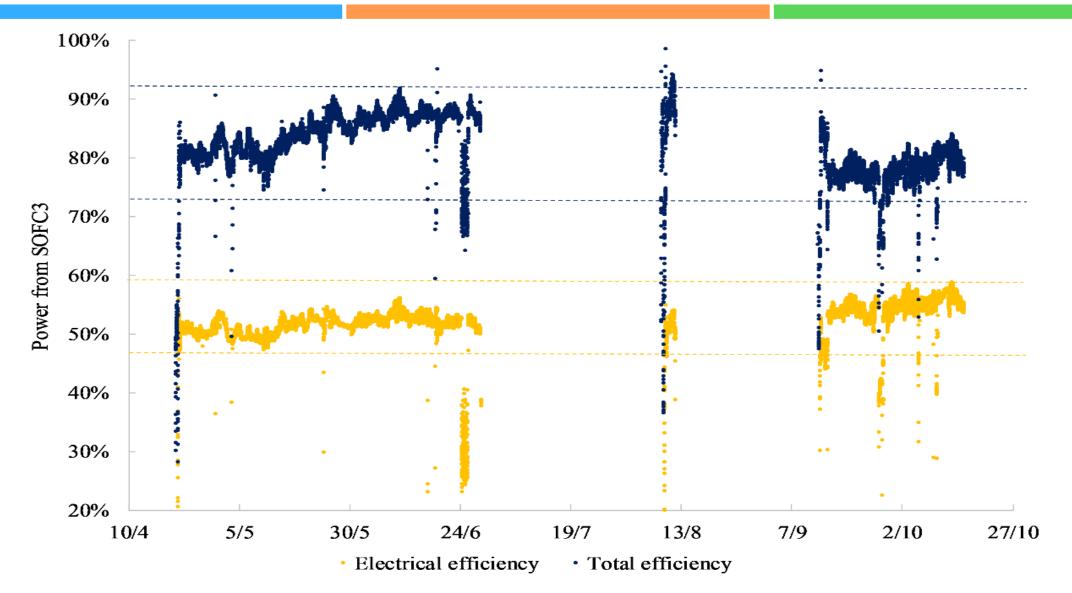
#### **SOFC Electrical Power production – Module 1**





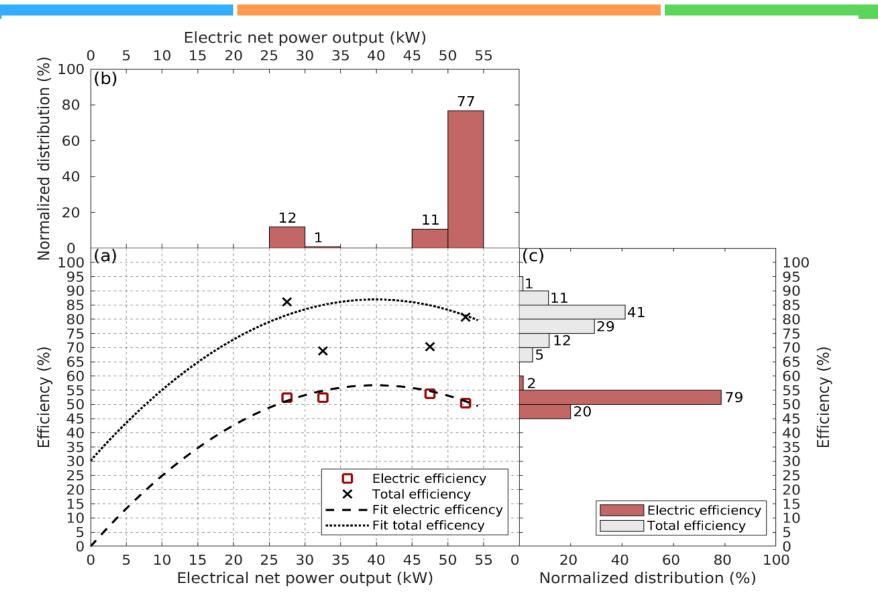
#### SOFC electrical and global efficiency – Module 1





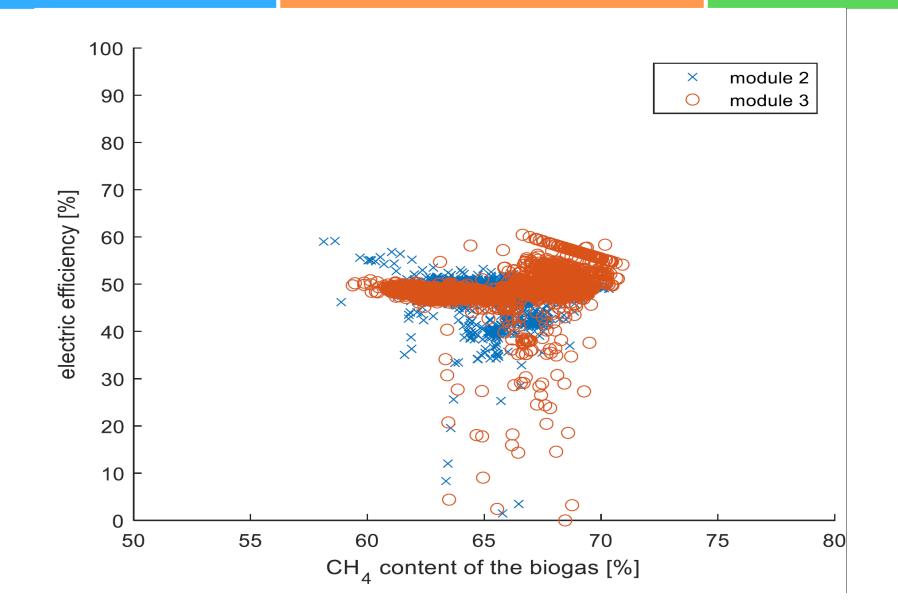
#### **SOFC efficiency – Module 1**





#### SOFC electrical efficiency vs %CH4





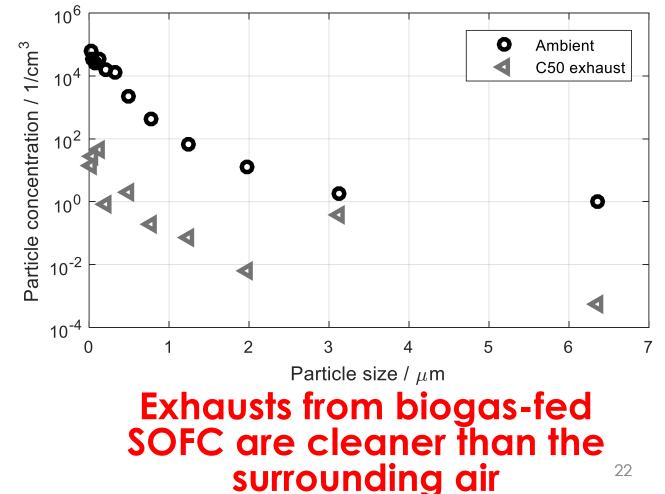
#### Some results: emissions





Species	Unit	Measured value
H <sub>2</sub> O	Vol-%	4.7
CO <sub>2</sub>	Vol-%	3.4
СО	mg/m <sup>3</sup>	<9
CH <sub>4</sub>	mg/m <sup>3</sup>	<2
N <sub>2</sub> O	mg/m <sup>3</sup>	<8
NO	mg/m <sup>3</sup>	<20
$NO_x$ (as $NO_2$ )	mg/m <sup>3</sup>	<20
SO <sub>2</sub>	mg/m <sup>3</sup>	<8
C <sub>2</sub> H <sub>6</sub>	mg/m <sup>3</sup>	<14
НСНО	mg/m <sup>3</sup>	<7
HF	mg/m <sup>3</sup>	<10
HCI	mg/m <sup>3</sup>	<10
SO <sub>2</sub>	mg/m <sup>3</sup>	<10
O <sub>2</sub>	Vol-%	18.3
Particulate	mg/m3	0.01

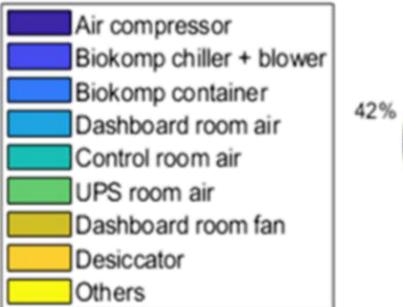
# Particulate emission during steady state

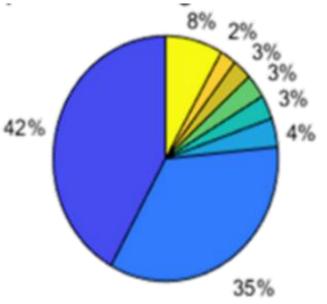


## **SOFC auxiliary consumption**



#### OVER A TOTAL PRODUCTION OF AROUND 110 kW





The total auxiliary consumption (including all the biogas treatment section, heat recovery, electrical and control parts, conditioning of the technical building, etc.) is around 11.72 kW.

The value is dominated by the biogas treatment section (two chillers, blower, compressor) and all the equipment within the container (especially ventilation and cooling during Summer). The two sections together account for 77% of the consumption.

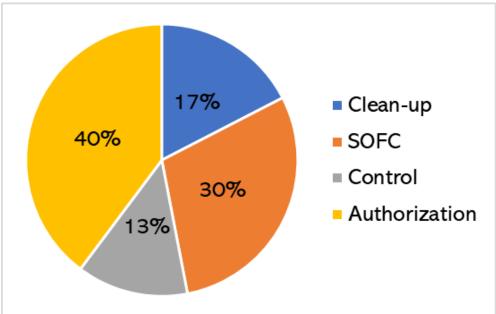
## Capacity factor and stops of the plant



	Hours ON - h	Electrical Energy - kWh	Capacity factor - %
Tot. SOFC1	6,537	283,376	46.64%
Tot. SOFC2	7,710	320,115	67.70%
Tot. DEMOSOFC	14,247	603,492	55.00%

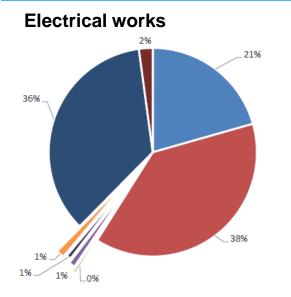
#### → OFF periods were due to:

- Cleaning system → freezing problem at the beginning (then solved), planned (every 6'000 hours) and unplanned maintenance on the biogas compressor and blower.
- SOFC → air pre-heater maintenance, island mode testing and checking, maintenance on stack module 1.
- Control system → in the first 6-8 months the software was finalized and updated based on the experience gained onsite.
- Authorization 
   → time required to renew the authorization
   and install the power meter requested

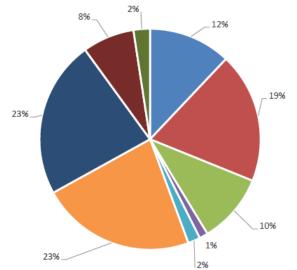


#### **Economics**





#### Mechanical works



#### Electrical cabinet

Main grounded duct

- SOFC's electric connections
- Clean up's electric connections
- CONVION interface cabinet
- Secondary grounded duct

Primary circulation pumps

Sludges warming

Compressed air

Cost of labour

Additional works

Safety cost

Secondary circulation pumps

Heating of Technical water

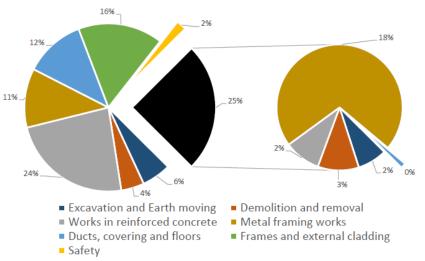
Biogas and technical gases

- PLC
- Optical fiber

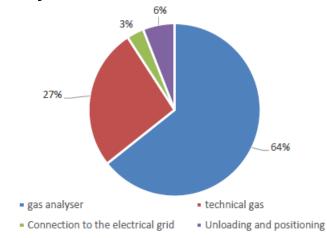
Mechanical 174.562 Works Electrical 173.913 Works **Civil Works** 191.920 Clean-up 221.087 system Auxiliary 91.677 works TOTAL 853.159

Actual Cost [€]

#### **Civil works**



#### **Auxiliary works**



25

#### **Economics**



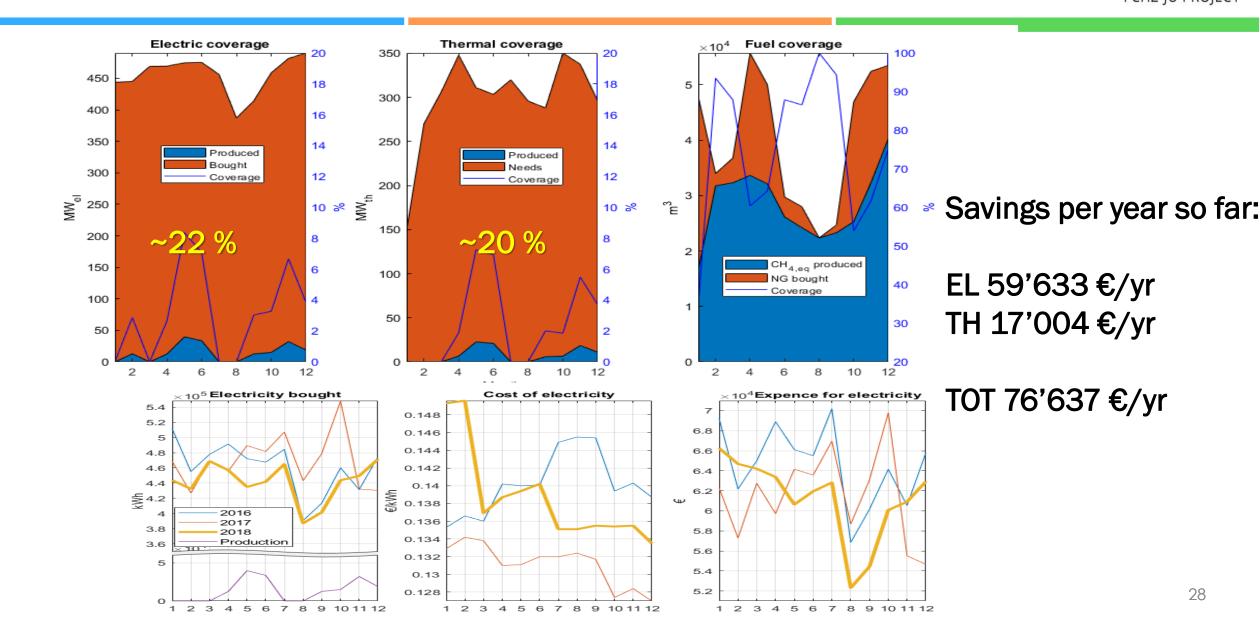
#### **Plant optimization analysis:**

- Moving from underground pipeline to external (covered) pipeline
- Removal of twin pumps
- Reduction of UPS size
- Simplification of the technical building (→ containerized solution)
- Optimization of the cleaning system

	Actual Cost [€]	Estimated Cost [€]	Reduction
Mechanical Works	174.562	65.502	-63%
Electrical Works	173.913	100.819	-42%
Civil Works	191.920	23758	-88%
Clean-up system	221.087	132.652	-40%
Auxiliary works	91.677	54.597	-40%
TOTAL	853.159	377.328	-56%

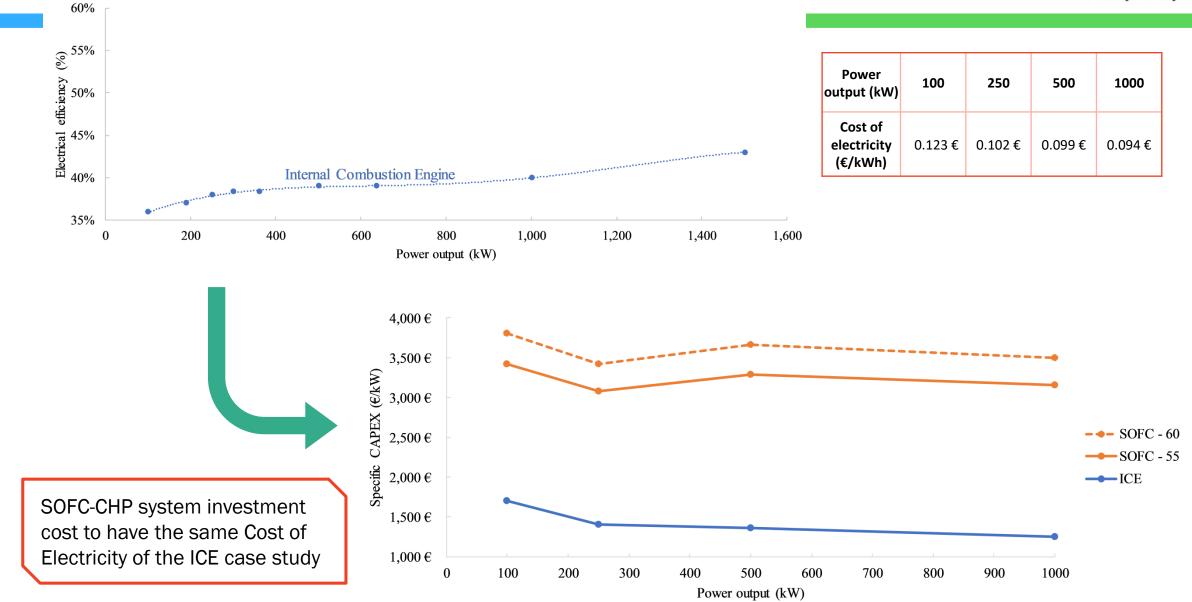
Future perspectives for SOFC in the WWTP sector and some economic considerations

## SOFC energy coverage and cost savings in the WWTP



#### Which should be the price of an SOFC system in a WWTP?

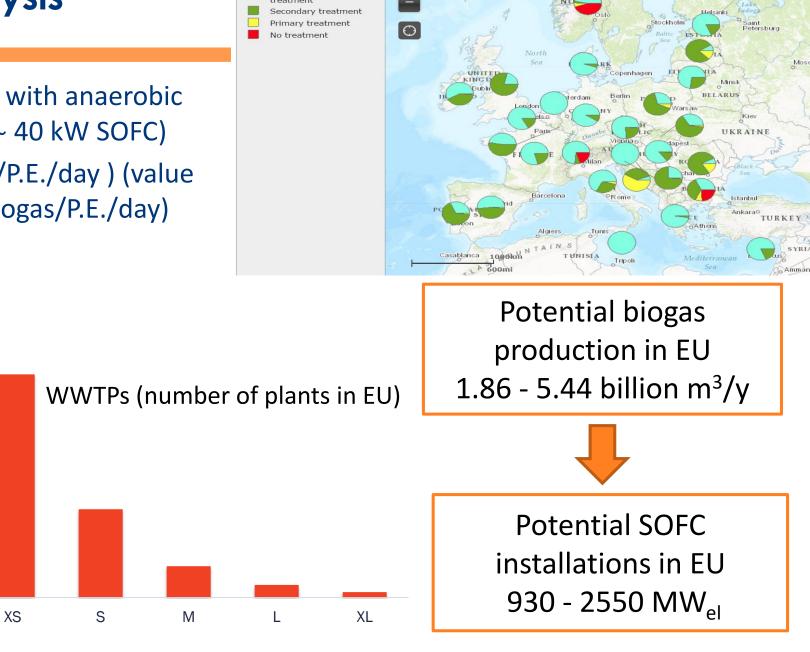




## Potential markets analysis

- → Minimum entering load for WWTP with anaerobic digestion: 20'000 P.E. (20'000 P.E. ~ 40 kW SOFC)
- → Biogas specific production: 10-29 I/P.E./day ) (value for conservative calculation: 10 I biogas/P.E./day)
- → Methane content: 60%
- → Capacity factor: 95%
- → SOFC electrical efficiency: 53%





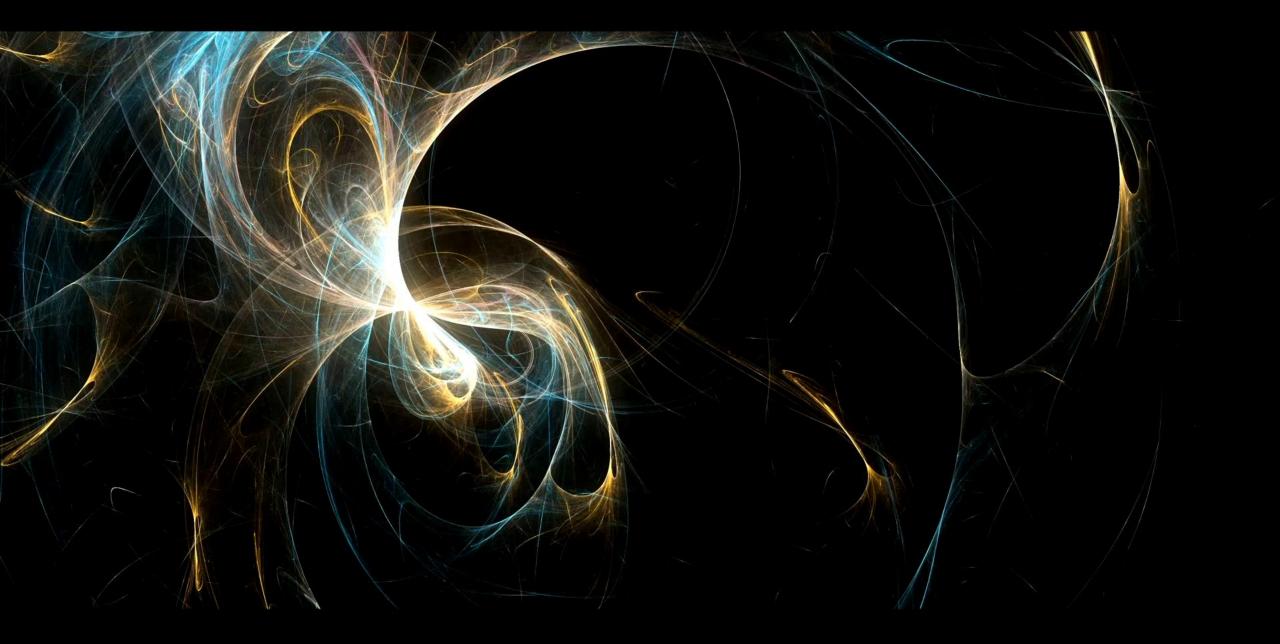
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FINLAND

UWWTD treatment plants UWWTD treatment plants No. of UWWT plants by treatment type by Member State

lore stringent







FCH2-JU PROJECT

## Thank you!

#### Prof. Massimo Santarelli, PhD Department of Energy, Politenico di Torino (IT)

DEMOSOFC has an overall budget of 5.9 million of euro and is receiving 4.2 million euro funding from the Fuel Cells and Hydrogen 2 Joint Undertaking under grant agreement No 671470. This Joint Undertaking receives support from the European Union's Horizon 2020 research and innovation programme, Hydrogen Europe and Hydrogen Europe research. The project is coordinated by the Energy Department of Politecnico di Torino (IT). The partners are: SMAT (IT), Convion Oy (FI), VTT Research Center (FI), Imperial College of Science Technology and Medicine (UK).



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CONVION

POLITECNICO DI TORINO



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